

HYSYS Chemical Process Simulation, Monell 20
(May 3, 2007)
[regenerated November 11, 2024]

Stream #	1	2	3	4	5	6	7
Vapour Fraction	1.000	1.000	0.999	1.000	1.000	0.000	0.000
Temperature, F	104.0	104.0	30.0	4.6	77.7	200.1	120.0
Pressure, psig	345.0	340.0	335.0	330.0	325.0	340.0	335.0
Molar Flow, MMSCFD	17.07	17.00	17.00	16.83	16.83	0.17	0.17
Mass Flow, lb/hr	80969	80832	80832	79692	79692	1139	1139
Liquid Volume Flow, USGPM	-	-	-	-	-	3.769	3.768989
Heat Flow, btu/hr	-3.024E+08	-3.016E+08	-3.032E+08	-3.025E+08	-3.009E+08	-1.262E+06	-1.323E+06
Composition, mol%							
H2S	0.0031	0.0031	0.0031	0.0030	0.0030	0.0094	0.0094
Nitrogen	0.0008	0.0008	0.0008	0.0008	0.0008	0.0000	0.0000
CO2	0.9362	0.9400	0.9400	0.9492	0.9492	0.0500	0.0500
Methane	0.0218	0.0219	0.0219	0.0221	0.0221	0.0000	0.0000
Ethane	0.0155	0.0156	0.0156	0.0158	0.0158	0.0000	0.0000
Propane	0.0116	0.0116	0.0116	0.0088	0.0088	0.2791	0.2791
i-Butane	0.0015	0.0015	0.0015	0.0002	0.0002	0.1285	0.1285
n-Butane	0.0031	0.0031	0.0031	0.0001	0.0001	0.2978	0.2978
i-Pentane	0.0007	0.0007	0.0007	0.0000	0.0000	0.0685	0.0685
n-Pentane	0.0006	0.0006	0.0006	0.0000	0.0000	0.0587	0.0587
n-Hexane	0.0005	0.0005	0.0005	0.0000	0.0000	0.0489	0.0489
n-Octane	0.0006	0.0006	0.0006	0.0000	0.0000	0.0587	0.0587
H2O	0.0041	0.0000	0.0000	0.0000	0.0000	0.0004	0.0004

1
2 Apache Inlet
3 1
4 Overhead
5 Residue
6 Bottoms
7 To Tanks

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Stream #	8	9	10	11	12	13	14
Vapour Fraction	0.000	0.000	1.000	1.000	1.000	1.000	1.000
Temperature, F	120.1	115.3	100.0	100.0	264.3	120.0	-5.1
Pressure, psig	200.3	185.3	5.3	4.3	635.3	630.3	20.0
Molar Flow, MMSCFD	0.17	0.16	0.01	0.01	0.01	0.01	10.87
Mass Flow, lb/hr	1139	1091	48	48	48	48	52656
Liquid Volume Flow, USGPM	3.768989	3.6804666	-	-	-	-	-
Heat Flow, btu/hr	-1.323E+06	-1.160E+06	-1.628E+05	-1.628E+05	-1.616E+05	-1.635E+05	-5.517E+07
Composition, mol%							
H2S	0.0094	0.0000	0.1580	0.1580	0.1580	0.1580	0.0000
Nitrogen	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
CO2	0.0500	0.0000	0.8420	0.8420	0.8420	0.8420	0.0000
Methane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Ethane	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
Propane	0.2791	0.2968	0.0000	0.0000	0.0000	0.0000	1.0000
i-Butane	0.1285	0.1366	0.0000	0.0000	0.0000	0.0000	0.0000
n-Butane	0.2978	0.3166	0.0000	0.0000	0.0000	0.0000	0.0000
i-Pentane	0.0685	0.0728	0.0000	0.0000	0.0000	0.0000	0.0000
n-Pentane	0.0587	0.0624	0.0000	0.0000	0.0000	0.0000	0.0000
n-Hexane	0.0489	0.0520	0.0000	0.0000	0.0000	0.0000	0.0000
n-Octane	0.0587	0.0624	0.0000	0.0000	0.0000	0.0000	0.0000
H2O	0.0004	0.0004	0.0000	0.0000	0.0000	0.0000	0.0000

8 Cool To Tanks
9 Treated Product
10 Acid Gas
11 Acid Gas In
12 AG 3 Out
13
14 Cond to Suct

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Stream #	15	16	17
Vapour Fraction	1.000	0.000	0.327
Temperature, F	158.4	120.0	1.7
Pressure, psig	235.3	230.3	25.0
Molar Flow, MMSCFD	13.02	13.02	10.87
Mass Flow, lb/hr	63041	63041	52656
Liquid Volume Flow, USGPM	-	-	139.37645
Heat Flow, btu/hr	-6.279E+07	-7.178E+07	-6.117E+07
Composition, mol%			
H2S	0.0000	0.0000	0.0000
Nitrogen	0.0000	0.0000	0.0000
CO2	0.0000	0.0000	0.0000
Methane	0.0000	0.0000	0.0000
Ethane	0.0000	0.0000	0.0000
Propane	1.0000	1.0000	1.0000
i-Butane	0.0000	0.0000	0.0000
n-Butane	0.0000	0.0000	0.0000
i-Pentane	0.0000	0.0000	0.0000
n-Pentane	0.0000	0.0000	0.0000
n-Hexane	0.0000	0.0000	0.0000
n-Octane	0.0000	0.0000	0.0000
H2O	0.0000	0.0000	0.0000

15 Comp Disc
16 Cool Disc
17 To Cond